Influence of the first-order contributions to the partial temperatures on transport properties in polydisperse dense granular mixtures

Rubén Gómez González[®]

Departamento de Física, Universidad de Extremadura, E-06006 Badajoz, Spain

Vicente Garzó 1

Departamento de Física and Instituto de Computación Científica Avanzada (ICCAEx), Universidad de Extremadura, E-06006 Badajoz, Spain

(Received 18 July 2019; published 19 September 2019)

The Chapman-Enskog solution to the Enskog kinetic equation of polydisperse granular mixtures is revisited to determine the first-order contributions ϖ_i to the partial temperatures. As expected, these quantities (which were neglected in previous attempts) are given in terms of the solution to a set of coupled integrodifferential equations analogous to those for elastic collisions. The solubility condition for this set of equations is confirmed and the coefficients ϖ_i are calculated by using the leading terms in a Sonine polynomial expansion. These coefficients are given as explicit functions of the sizes, masses, composition, density, and coefficients of restitution of the mixture. Within the context of small gradients, the results apply for arbitrary degrees of inelasticity and are not restricted to specific values of the parameters of the mixture. In the case of elastic collisions, previous expressions of ϖ_i for ordinary binary mixtures are recovered. Finally, the impact of the first-order coefficients ϖ_i on the bulk viscosity η_b and on the first-order contribution $\zeta^{(1)}$ to the cooling rate is assessed. It is shown that the effect of ϖ_i on η_b and $\zeta^{(1)}$ is not negligible, specially for disparate mass ratios and strong inelasticity.

DOI: 10.1103/PhysRevE.100.032904

I. INTRODUCTION

The understanding of transport processes occurring in polydisperse granular mixtures (namely, a mixture of smooth hard spheres with inelastic collisions) is still an exciting unsolved problem [1-3]. The reason for this challenging target is twofold: first, there is a large number of relevant parameters involved in the description of the granular mixtures; and second, there is a wide array of intricacies arising in the derivation of kinetic theory models. Thus, to gain some insight into the problem, the two most common simplifications employed in many of the pioneering papers on granular mixtures [4–8] were (i) to consider mixtures constituted by nearly elastic particles and (ii) to assume the equipartition of the total granular kinetic energy in the homogeneous cooling state (namely, they assume that the zeroth-order contributions $T_i^{(0)}$ to the partial temperatures T_i of each species are equal to the granular temperature T). On the other hand, the last assumption can be only justified for quasielastic collisions since the failure of energy equipartition in granular fluids [9,10] has been confirmed by computer simulations [11-18]and observed in real experiments of agitated granular mixtures [19,20]. The above papers have also shown that the departure of energy equipartition depends on the mechanical differences

*ruben@unex.es

among the particles and the coefficients of restitution of the granular mixture.

The inclusion of energy nonequipartition effects on transport in granular mixtures has been considered in more recent papers of dilute [21–26] and moderate [27–29] densities. In particular, the results derived from the inelastic Enskog equation [27–29] cover some of the aspects not accounted for in previous studies. More specifically, (i) they are expected to be applicable for a wide range of coefficients of restitution (since they take into account the nonlinear dependence of the transport coefficients on the coefficients of restitution); (ii) they consider the impact of nonequipartition of granular energy on the Navier-Stokes transport coefficients; and (iii) they are valid for moderate densities. Thus, these works [27–29] subsume all previous studies for dilute [21–26] and dense quasielastic [4–8] granular mixtures, which are recovered in the appropriate limits.

Nevertheless, the theory developed for dense gases [27–29] is based on a simplifying assumption. Although not explicitly stated, the results derived in Refs. [27–29] were obtained by neglecting the first-order contributions $T_i^{(1)}$ to the partial temperatures T_i . The existence of a nonzero first-order contribution $T_i^{(1)}$ induces a breakdown of the energy equipartition, additional to the one appearing in the homogeneous cooling state (which is only due to the inelastic character of collisions). In fact, $T_i^{(1)} \neq 0$ in the case of ordinary dense mixtures (namely, a dense hard-sphere mixture with elastic collisions). Although the partial temperatures are not hydrodynamic quantities, their determination is interesting in itself. In addition, a careful analysis of the first-order contributions to the collisional part P^c of the pressure tensor and the cooling rate ζ (which

[†]vicenteg@unex.es; http://www.unex.es/eweb/fisteor/vicente/

accounts for the rate of kinetic energy dissipation due to inelastic collisions) shows that there are contributions to P^c and ζ coming from the coefficients $T_i^{(1)}$. Since the first-order contributions to the partial temperatures are proportional to the divergence of the flow velocity **U**, then the coefficients $T_i^{(1)}$ are involved in the evaluation of both the bulk viscosity η_b (proportionality coefficient between P^c and $\nabla \cdot \mathbf{U}$) and the first-order contribution ζ_U to the cooling rate (proportionality coefficient between ζ and $\nabla \cdot \mathbf{U}$). The coupling between $T_i^{(1)}$ and η_b was in fact already recognized in the pioneering papers [30–32] of the Enskog theory for multicomponent ordinary mixtures.

The question arises then as to whether, and if so to what extent, the conclusions drawn from Refs. [27–29] for η_b and ζ may be altered when the above new ingredient (first-order contributions to the partial temperatures) is accounted for in the theory. In this paper we calculate $T_i^{(1)}$ and assess the impact of these coefficients on η_b and ζ for granular mixtures.

The plan of the paper is as follows. The Enskog kinetic equation for polydisperse granular mixtures is introduced in Sec. II and the corresponding balance equations for the densities of mass, momentum, and energy are recalled. Section III deals with the evaluation of the first-order contributions to the partial temperatures. As expected, the coefficients $T_i^{(1)}$ are given in terms of the solution to a set of linear integral equations. The leading term in a Sonine polynomial expansion is retained in Sec. IV to solve the above set and obtain the partial temperatures in terms of the parameter space of the

problem. For the sake of illustration, a binary mixture is considered in Sec. V. The results show that the impact of the coefficients $T_i^{(1)}$ on both the bulk viscosity and the cooling rate is not in general negligible and must be accounted for, specially for disparate mass ratios and strong dissipation. The paper closes in Sec. VI with some concluding remarks.

II. ENSKOG KINETIC EQUATION FOR POLYDISPERSE DENSE GRANULAR MIXTURES

We consider an *s*-component granular mixture of inelastic hard disks (d = 2) or spheres (d = 3) of masses m_i and diameters σ_i . The subscript *i* labels one of the *s* mechanically different components and *d* is the dimension of the system. Spheres are assumed to be completely smooth so that the inelasticity of collisions is only characterized by the constant (positive) coefficients of restitution $\alpha_{ij} \leq 1$. The mixture is also assumed to be in the presence of the gravitational field and hence, each particle feels the action of the force $\mathbf{F}_i = m_i \mathbf{g}$, where \mathbf{g} is the gravity acceleration. For moderate densities, the one-particle velocity distribution function $f_i(\mathbf{r}, \mathbf{v}, t)$ of component *i* verifies the set of *s*-coupled nonlinear integrodifferential Enskog equations:

$$\frac{\partial f_i}{\partial t} + \mathbf{v} \cdot \nabla f_i + \mathbf{g} \cdot \frac{\partial f_i}{\partial \mathbf{v}} = \sum_{j=1}^s J_{ij}[\mathbf{r}, \mathbf{v}|f_i, f_j], \qquad (1)$$

where the Enskog collision operator is [3]

$$J_{ij}[\mathbf{r}_{1},\mathbf{v}_{1}|f_{i},f_{j}] = \sigma_{ij}^{d-1} \int d\mathbf{v}_{2} \int d\widehat{\boldsymbol{\sigma}} \Theta(\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) (\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) [\alpha_{ij}^{-2} \chi_{ij}(\mathbf{r}_{1},\mathbf{r}_{1}-\sigma_{ij})f_{i}(\mathbf{r}_{1},\mathbf{v}_{1}'',t)f_{j}(\mathbf{r}_{1}-\sigma_{ij},\mathbf{v}_{2}'',t) - \chi_{ij}(\mathbf{r}_{1},\mathbf{r}_{1}+\sigma_{ij})f_{i}(\mathbf{r}_{1},\mathbf{v}_{1},t)f_{j}(\mathbf{r}_{1}+\sigma_{ij},\mathbf{v}_{2},t)].$$

$$(2)$$

In Eq. (1), $\sigma_{ij} = \sigma_{ij}\hat{\sigma}$, $\sigma_{ij} = (\sigma_i + \sigma_j)/2$, $\hat{\sigma}$ is a unit vector directed along the line of centers from the sphere of component *i* to that of component *j* at contact, Θ is the Heaviside step function, and $\mathbf{g}_{12} = \mathbf{v}_1 - \mathbf{v}_2$ is the relative velocity of the colliding pair. Moreover, $\chi_{ij}(\mathbf{r}_1, \mathbf{r}_1 + \sigma_{ij})$ is the equilibrium pair correlation function of two hard spheres, one of component *i* and the other of component *j* at contact, i.e., when the distance between their centers is σ_{ij} . The precollisional velocities $(\mathbf{v}''_1, \mathbf{v}''_2)$ are given by

$$\mathbf{v}_{1}^{\prime\prime} = \mathbf{v}_{1} - \mu_{ji} \big(1 + \alpha_{ij}^{-1} \big) (\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) \widehat{\boldsymbol{\sigma}}, \qquad (3)$$

$$\mathbf{v}_{2}^{\prime\prime} = \mathbf{v}_{2} + \mu_{ij} \left(1 + \alpha_{ij}^{-1} \right) (\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) \widehat{\boldsymbol{\sigma}}, \tag{4}$$

where $\mu_{ij} = m_i / (m_i + m_j)$.

The first few velocity moments of the distributions f_i define the hydrodynamic fields of the mixture. Thus, the local number density of component *i* is

$$n_i = \int d\mathbf{v} \ f_i(\mathbf{v}),\tag{5}$$

while the local mean flow velocity of grains is defined as

$$\mathbf{U} = \rho^{-1} \sum_{i=1}^{s} \int d\mathbf{v} \ m_i \mathbf{v} f_i(\mathbf{v}), \tag{6}$$

where $\rho = \sum_{i} m_{i}n_{i}$ is the total mass density. Apart from the partial densities n_{i} and the flow velocity **U**, the other important hydrodynamic field is the granular temperature *T*. It is defined as

$$T = \frac{1}{n} \sum_{i=1}^{s} \int d\mathbf{v} \frac{m_i}{d} V^2 f_i(\mathbf{v}), \tag{7}$$

where $n = \sum_{i} n_i$ is the total number density and $\mathbf{V} = \mathbf{v} - \mathbf{U}$ is the peculiar velocity. At a kinetic level, it is also convenient to introduce the partial kinetic temperatures T_i for each component. These quantities measure the mean kinetic energy of each component. They are defined as

$$T_i = \frac{m_i}{dn_i} \int d\mathbf{v} \, V^2 f_i(\mathbf{v}). \tag{8}$$

According to Eq. (7), the granular temperature T of the mixture can be also written as

$$T = \sum_{i=1}^{s} x_i T_i,\tag{9}$$

where $x_i = n_i/n$ is the mole fraction of component *i*.

An important property of the integrals involving the Enskog collision operator $J_{ij}[\mathbf{r}, \mathbf{v}|f_i, f_j]$ is [3,27]

$$I_{\psi_{i}} \equiv \sum_{i,j=1}^{s} \int d\mathbf{v}_{1} \ \psi_{i}(\mathbf{v}_{1}) J_{ij}[\mathbf{r}_{1}, \mathbf{v}_{1}|f_{i}, f_{j}]$$

$$= \frac{1}{2} \sum_{i,j=1}^{s} \sigma_{ij}^{d-1} \int d\mathbf{v}_{1} \int d\mathbf{v}_{2} \int d\widehat{\boldsymbol{\sigma}} \ \Theta(\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) (\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) \Big\{ \Big[\psi_{i}(\mathbf{v}_{1}') + \psi_{j}(\mathbf{v}_{2}') - \psi_{i}(\mathbf{v}_{1}) - \psi_{j}(\mathbf{v}_{2}) \Big] f_{ij}(\mathbf{r}_{1}, \mathbf{v}_{1}, \mathbf{r}_{2}, \mathbf{v}_{2}; t)$$

$$+ \frac{\partial}{\partial \mathbf{r}_{1}} \cdot \sigma_{ij} \Big[\psi_{i}(\mathbf{v}_{1}') - \psi_{i}(\mathbf{v}_{1}) \Big] \int_{0}^{1} dx \ f_{ij}(\mathbf{r}_{1} - x\sigma_{ij}, \mathbf{v}_{1}, \mathbf{r}_{1} + (1 - x)\sigma_{ij}, \mathbf{v}_{2}; t) \Big\},$$
(10)

where

$$f_{ij}(\mathbf{r}_1, \mathbf{v}_1, \mathbf{r}_2, \mathbf{v}_2; t) \equiv \chi_{ij}(\mathbf{r}_1, \mathbf{r}_2) f_i(\mathbf{r}_1, \mathbf{v}_1, t) f_j(\mathbf{r}_2, \mathbf{v}_2, t),$$
(11)

 $\psi_i(\mathbf{v}_1)$ is an arbitrary function of \mathbf{v}_1 , and

$$\mathbf{v}_1' = \mathbf{v}_1 - \mu_{ji}(1 + \alpha_{ij})(\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12})\widehat{\boldsymbol{\sigma}}.$$
(12)

The first term on the right-hand side of Eq. (10) represents a collisional effect due to scattering with a change in velocities. The second term provides a pure collisional effect due to the spatial difference of the colliding pair. For elastic collisions, the first term vanishes. The balance equations for the densities of mass, momentum, and energy can be derived by using the property (10). They are given by [3]

$$D_t n_i + n_i \nabla \cdot \mathbf{U} + \frac{\nabla \cdot \mathbf{j}_i}{m_i} = 0,$$
(13)

$$D_t \mathbf{U} + \rho^{-1} \nabla \cdot \mathbf{P} = \mathbf{g},\tag{14}$$

$$D_t T - \frac{T}{n} \sum_{i=1}^s \frac{\nabla \cdot \mathbf{j}_i}{m_i} + \frac{2}{dn} (\nabla \cdot \mathbf{q} + \mathbf{P} : \nabla \mathbf{U}) = -\zeta T.$$
(15)

In the above equations, $D_t = \partial_t + \mathbf{U} \cdot \nabla$ is the material derivative, $\rho_i = m_i n_i$ is the mass density of component *i*, and

$$\mathbf{j}_i = m_i \int d\mathbf{v} \, \mathbf{V} f_i(\mathbf{v}) \tag{16}$$

is the mass flux for component *i* relative to the local flow U. A consequence of the definition (16) of the fluxes \mathbf{j}_i is that

$$\sum_{i=1}^{s} \mathbf{j}_i = \mathbf{0},\tag{17}$$

and hence, only s - 1 mass fluxes are independent. The pressure tensor $P(\mathbf{r}, t)$ and the heat flux $q(\mathbf{r}, t)$ have both kinetic and collisional transfer contributions, i.e.,

$$\mathbf{P} = \mathbf{P}^{k} + \mathbf{P}^{c}, \quad \mathbf{q} = \mathbf{q}^{k} + \mathbf{q}^{c}.$$
(18)

The kinetic contributions P^k and q^k are given by

$$\mathbf{P}^{\mathbf{k}} = \sum_{i=1}^{s} \int d\mathbf{v} \ m_i \mathbf{V} \mathbf{V} f_i(\mathbf{v}), \tag{19}$$

$$\mathbf{q}^{\mathbf{k}} = \sum_{i=1}^{s} \int d\mathbf{v} \, \frac{m_i}{2} V^2 \mathbf{V} f_i(\mathbf{v}). \tag{20}$$

The collisional transfer contributions are [3,27]

$$\mathbf{P}^{c} = \sum_{i,j=1}^{s} \sigma_{ij}^{d} m_{ij} \frac{1+\alpha_{ij}}{2} \int d\mathbf{v}_{1} \int d\mathbf{v}_{2} \int d\widehat{\boldsymbol{\sigma}} \Theta(\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) (\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12})^{2} \widehat{\boldsymbol{\sigma}} \widehat{\boldsymbol{\sigma}} \int_{0}^{1} dx f_{ij} (\mathbf{r} - x \sigma_{ij}, \mathbf{r} + (1-x)\sigma_{ij}, \mathbf{v}_{1}, \mathbf{v}_{2}, t), \quad (21)$$

$$\mathbf{q}^{c} = \sum_{i,j=1}^{s} \sigma_{ij}^{d} m_{ij} \frac{1+\alpha_{ij}}{8} \int d\mathbf{v}_{1} \int d\mathbf{v}_{2} \int d\widehat{\boldsymbol{\sigma}} \Theta(\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) (\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12})^{2} \widehat{\boldsymbol{\sigma}} [4(\widehat{\boldsymbol{\sigma}} \cdot \mathbf{G}_{ij}) + (\mu_{ji} - \mu_{ij})(1-\alpha_{ij})(\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12})] \int_{0}^{1} dx f_{ij} (\mathbf{r} - x \sigma_{ij}, \mathbf{r} + (1-x)\sigma_{ij}, \mathbf{v}_{1}, \mathbf{v}_{2}; t). \quad (22)$$

Here, $m_{ij} = m_i m_j / (m_i + m_j)$ is the reduced mass and $\mathbf{G}_{ij} = \mu_{ij} \mathbf{V}_1 + \mu_{ji} \mathbf{V}_2$ is the velocity of the center of mass. Finally, the (total) cooling rate ζ due to inelastic collisions among all components is given by

$$\zeta = \frac{1}{2dnT} \sum_{i,j=1}^{s} \sigma_{ij}^{d-1} m_{ij} \left(1 - \alpha_{ij}^{2}\right) \int d\mathbf{v}_{1} \int d\mathbf{v}_{2} \int d\widehat{\boldsymbol{\sigma}} \Theta(\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) (\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12})^{3} f_{ij}(\mathbf{r}, \mathbf{r} + \boldsymbol{\sigma}_{ij}, \mathbf{v}_{1}, \mathbf{v}_{2}; t).$$
(23)

As expected, the balance equations (13)–(15) are not a closed set of equations for the fields n_i , **U**, and *T*. To transform these equations into a set of closed equations, one has to express the fluxes and the cooling rate in terms of the hydrodynamic fields and their gradients. The corresponding constitutive equations can be obtained by solving the set of Enskog kinetic equations (1) with the Chapman-Enskog method [33] adapted to dissipative dynamics.

III. FIRST-ORDER CONTRIBUTIONS TO THE PARTIAL TEMPERATURES

The inelastic Enskog equation (1) was solved in Refs. [27,28] by means of the Chapman-Enskog method. In particular, the first-order velocity distribution functions $f_i^{(1)}$ are given by [27]

$$f_{i}^{(1)} = \mathcal{A}_{i} \cdot \nabla \ln T + \sum_{j=1}^{s} \mathcal{B}_{ij} \cdot \nabla \ln n_{j} + \mathcal{C}_{i,\lambda\beta} \frac{1}{2} \left(\partial_{\lambda} U_{\beta} + \partial_{\beta} U_{\lambda} - \frac{2}{d} \delta_{\lambda\beta} \nabla \cdot \mathbf{U} \right) + \mathcal{D}_{i} \nabla \cdot \mathbf{U},$$
(24)

where $\partial_{\lambda} \equiv \partial/\partial r_{\lambda}$. The unknowns $\mathcal{A}_i(\mathbf{V})$, $\mathcal{B}_{ij}(\mathbf{V})$, $\mathcal{C}_{i,\lambda\beta}(\mathbf{V})$, and $\mathcal{D}_i(\mathbf{V})$ are functions of the peculiar velocity \mathbf{V} and they are the solutions of a set of coupled linear integral equations [27]. Approximate solutions to this set of integral equations were obtained in Refs. [28,29] by considering the leading terms in a Sonine polynomial expansion. This procedure allows us to obtain explicit forms of the Navier-Stokes transport coefficients in terms of the mechanical parameters of the mixture (masses and sizes and the coefficients of restitution), the composition, and the density. Within the context of small gradients, the results apply in principle for arbitrary values of the coefficients of restitution and a wide range of densities.

However, as said in Sec. I, the influence of the firstorder contribution $T_i^{(1)}$ to T_i on the transport coefficients was neglected in the above papers [27,28]. This was essentially assumed because $T_i^{(1)}$ comes from the second-Sonine approximation and hence it is expected that its impact on transport properties is small. Here, we want to determine $T_i^{(1)}$ to assess its influence on the bulk viscosity and the cooling rate.

According to Eq. (8), the first-order contribution to the partial temperature T_i is defined as

$$T_i^{(1)} = \frac{m_i}{dn_i} \int d\mathbf{v} \, V^2 f_i^{(1)}(\mathbf{V}).$$
(25)

Since $T_i^{(1)}$ is a scalar, it can be only coupled to the divergence of the flow velocity $\nabla \cdot \mathbf{U}$ since ∇n and ∇T are vectors and $\partial_{\lambda}U_{\beta} + \partial_{\beta}U_{\lambda} - (2/d)\delta_{\lambda\beta}\nabla \cdot \mathbf{U}$ is a traceless tensor. Thus, $T_i^{(1)}$ can be written as $T_i^{(1)} = \overline{\varpi}_i \nabla \cdot \mathbf{U}$, where

$$\overline{\varpi}_i = \frac{m_i}{dn_i} \int d\mathbf{v} \, V^2 \mathcal{D}_i(\mathbf{V}). \tag{26}$$

The fact that the total temperature *T* is not affected by the gradients implies necessarily the constraint $\sum_{i=1}^{s} n_i T_i^{(1)} = 0$. Thus, only s - 1 partial temperatures are independent. The above constraint comes directly from the solubility condition

$$\sum_{i=1}^{s} \int d\mathbf{v} m_i V^2 f_i^{(1)} = 0.$$
 (27)

As said before, apart from obtaining $T_i^{(1)}$, we are also interested here in revisiting previous calculations [27,28] made for the bulk viscosity η_b and the cooling rate ζ . The first coefficient has only collisional contributions and its form can be identified by expanding the collisional transfer contribution P^c to the pressure tensor to first order in spatial gradients. A careful first-order expansion of the expression (21) to P^c gives the following form for η_b :

$$\eta_{\rm b} = \eta_{\rm b}' + \eta_{\rm b}'',\tag{28}$$

where

$$\eta_{\rm b}' = \frac{\pi^{(d-1)/2}}{\Gamma(\frac{d+3}{2})} \frac{d+1}{2d^2} \sum_{i=1}^{s} \sum_{j=1}^{s} m_{ij}(1+\alpha_{ij})\chi_{ij}^{(0)}\sigma_{ij}^{d+1} \\ \times \int d\mathbf{v}_1 \int d\mathbf{v}_2 f_i^{(0)}(\mathbf{V}_1) f_j^{(0)}(\mathbf{V}_2) g_{12},$$
(29)

and

$$\eta_{\rm b}^{\prime\prime} = -\frac{\pi^{d/2}}{d\Gamma(\frac{d}{2})} \sum_{i=1}^{s} \sum_{j=1}^{s} \mu_{ji}(1+\alpha_{ij})\chi_{ij}^{(0)}n_in_j\sigma_{ij}^d\varpi_i.$$
 (30)

In Eq. (29), $f_i^{(0)}$ is the zeroth-order distribution. In addition, it is understood henceforth that the functional dependence of $\chi_{ij}^{(0)}(\mathbf{r}, \mathbf{r}' | \{n_i\})$ on the compositions to zeroth order in the gradients has the same functional dependence on the densities replaced by $\{n_i\} \rightarrow \{n_i(\mathbf{r}, t)\}$ at the point of interest.

The second contribution η_b' to η_b in Eq. (28) was neglected in previous works [3,27,28]. On the other hand, as said in Sec. I, the contribution η_b'' was already accounted for in the studies on ordinary (elastic collisions) hard-sphere mixtures [30–32] carried out many years ago. In fact, for elastic collisions, Eq. (30) is consistent with Eq. (18a) of Ref. [31].

In the case of the cooling rate, $\zeta \rightarrow \zeta^{(0)} + \zeta_U \nabla \cdot \mathbf{U}$ where

$$\begin{aligned} \boldsymbol{\zeta}^{(0)} &= \frac{1}{2dnT} \sum_{i,j=1}^{s} \sigma_{ij}^{d-1} m_{ij} \big(1 - \alpha_{ij}^2 \big) \boldsymbol{\chi}_{ij}^{(0)} \int d\mathbf{v}_1 \int d\mathbf{v}_2 \\ &\times \int d\widehat{\boldsymbol{\sigma}} \Theta(\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) (\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12})^3 f_i^{(0)}(\mathbf{r}, \mathbf{v}_1, t) f_j^{(0)}(\mathbf{r}, \mathbf{v}_2, t), \end{aligned}$$
(31)

and $\zeta_U = \zeta^{(1,0)} + \zeta^{(1,1)}$. Here,

$$\zeta^{(1,0)} = -\frac{3\pi^{d/2}}{d^2 \Gamma(\frac{d}{2})} \sum_{i=1}^{s} \sum_{j=1}^{s} x_i n_j \mu_{ji} \sigma_{ij}^d \chi_{ij}^{(0)} \gamma_i (1 - \alpha_{ij}^2),$$
(32)

and the coefficient $\zeta^{(1,1)}$ is given in terms of the unknowns \mathcal{D}_i as

$$\zeta^{(1,1)} = \frac{1}{nT} \frac{\pi^{(d-1)/2}}{d\Gamma\left(\frac{d+3}{2}\right)} \sum_{i=1}^{s} \sum_{j=1}^{s} \sigma_{ij}^{d-1} \chi_{ij}^{(0)} m_{ij} \left(1 - \alpha_{ij}^{2}\right) \int d\mathbf{v}_{1} \int d\mathbf{v}_{2} \ g_{12}^{3} \ f_{i}^{(0)}(\mathbf{V}_{1}) \mathcal{D}_{j}(\mathbf{V}_{2}).$$
(33)

In Eq. (32), $\gamma_i \equiv T_i^{(0)}/T$ is the temperature ratio of component *i*. The temperature ratios γ_i verify the relation $\sum_i x_i \gamma_i = 1$ and they are determined from the conditions $\zeta^{(0)} = \zeta_1^{(0)} = \zeta_2^{(0)} = \cdots = \zeta_s^{(0)}$, where

$$\zeta_i^{(0)} = -\frac{m_i}{dn_i T_i^{(0)}} \sum_{j=1}^s \int d\mathbf{v} V^2 J_{ij}^{(0)} [f_i^{(0)}, f_j^{(0)}].$$
(34)

According to the results obtained in Ref. [27], the coefficients ϖ_i are the solutions of the set of coupled linear integral equations

$$\frac{1}{2}\zeta^{(0)}\frac{\partial}{\partial \mathbf{V}}\cdot(\mathbf{V}\mathcal{D}_{i}) + \frac{1}{2}\zeta^{(0)}\mathcal{D}_{i} + \frac{1}{2}\zeta^{(1,1)}\frac{\partial}{\partial \mathbf{V}}\cdot(\mathbf{V}f_{i}^{(0)}) - \sum_{j=1}^{s}\left(J_{ij}^{(0)}\left[\mathcal{D}_{i},f_{j}^{(0)}\right] + J_{ij}^{(0)}\left[f_{i}^{(0)},\mathcal{D}_{j}\right]\right) = D_{i},$$
(35)

where

$$J_{ij}^{(0)}[f_i^{(0)}, f_j^{(0)}] = \chi_{ij}^{(0)} \sigma_{ij}^{d-1} \int d\mathbf{v}_2 \int d\widehat{\boldsymbol{\sigma}} \,\Theta(\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) (\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) [\alpha_{ij}^{-2} f_i^{(0)}(\mathbf{v}_1'') f_j^{(0)}(\mathbf{v}_2'') - f_i^{(0)}(\mathbf{v}_1) f_j^{(0)}(\mathbf{v}_2)]$$
(36)

is the Boltzmann collision operator multiplied by the (constant) pair distribution function $\chi_{ij}^{(0)}$, and D_i is given by

$$D_{i}(\mathbf{V}) = \frac{1}{2} \left[\frac{2}{d} (1 - p^{*}) - \zeta^{(1,0)} \right] \frac{\partial}{\partial \mathbf{V}} \cdot \left(\mathbf{V} f_{i}^{(0)} \right) - f_{i}^{(0)} + \sum_{j=1}^{s} \left(n_{j} \frac{\partial f_{i}^{(0)}}{\partial n_{j}} + \frac{1}{d} \mathcal{K}_{ij,\beta} \left[\frac{\partial f_{i}^{(0)}}{\partial V_{\beta}} \right] \right).$$
(37)

In addition, $\mathcal{K}_{ij}[X_j]$ is the collision operator

$$\mathcal{K}_{ij}[X_j] = \sigma_{ij}^d \chi_{ij}^{(0)} \int d\mathbf{v}_2 \int d\widehat{\boldsymbol{\sigma}} \Theta(\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) (\widehat{\boldsymbol{\sigma}} \cdot \mathbf{g}_{12}) \widehat{\boldsymbol{\sigma}} \Big[\alpha_{ij}^{-2} f_i^{(0)}(\mathbf{v}_1'') X_j(\mathbf{v}_2'') + f_i^{(0)}(\mathbf{v}_1) X_j(\mathbf{v}_2) \Big],$$
(38)

and the (reduced) hydrostatic pressure $p^* \equiv p/(nT)$ is

$$p^* = 1 + \frac{\pi^{d/2}}{d\Gamma(\frac{d}{2})} \sum_{i=1}^{s} \sum_{j=1}^{s} \mu_{ji} x_i x_j n \sigma_{ij}^d \chi_{ij}^{(0)} \gamma_i (1 + \alpha_{ij}).$$
(39)

Since $D_i(\mathbf{V}) \propto D_i(\mathbf{V})$, the solubility condition (27) requires necessarily that

$$\sum_{i=1}^{s} \int d\mathbf{v} m_i V^2 D_i(\mathbf{V}) = 0.$$
⁽⁴⁰⁾

This condition can easily be verified by direct integration of Eq. (37) and using Eqs. (32)–(39), the relation $\sum_i x_i \gamma_i = 1$, and the result

$$A_{i} \equiv \sum_{j=1}^{s} \int d\mathbf{v} m_{i} V^{2} \mathcal{K}_{ij,\lambda} \left[\frac{\partial f_{j}^{(0)}}{\partial V_{\lambda}} \right]$$

$$= -\frac{\pi^{d/2}}{\Gamma(\frac{d}{2})} T \sum_{j=1}^{s} \chi_{ij}^{(0)} n_{i} n_{j} \sigma_{ij}^{d} (1 + \alpha_{ij}) \left[3\mu_{ji} (1 + \alpha_{ij}) \times \left(\frac{\gamma_{i}}{m_{i}} + \frac{\gamma_{j}}{m_{j}} \right) - 4 \frac{\gamma_{i}}{m_{i}} \right].$$
(41)

In the low-density regime $(n_i \sigma_{ij}^d \to 0)$, $p^* = 1$, $\zeta^{(1,0)} = 0$, the combination $\sum_j n_j \partial f_i^{(0)} / \partial n_j - f_i^{(0)}$ and the operator $\mathcal{K}_{ij}[X_j]$ vanish, and so $D_i = 0$ in the integral equation (35). This means $\mathcal{D}_i = 0$ and hence, the first-order contributions ϖ_i to the partial temperatures vanish for *dilute* granular mixtures. This agrees with the previous results obtained in the low-density regime [21,22,24,25].

IV. LEADING SONINE APPROXIMATION

It is quite apparent that the calculation of ϖ_i requires one to solve the integral equation (35) as well as to know the zeroth-order distributions $f_i^{(0)}$. With respect to the latter, previous results [9,11] derived for homogeneous states have clearly shown that in the region of thermal velocities, $f_i^{(0)}$ is well represented by the Maxwellian velocity distribution defined at the lowest-order partial temperature $T_i^{(0)}$, namely,

$$f_i^{(0)}(\mathbf{V}) \to f_{i,\mathbf{M}}(\mathbf{V}) = n_i \left(\frac{m_i}{2\pi T_i^{(0)}}\right)^{d/2} \exp\left(-\frac{m_i V^2}{2T_i^{(0)}}\right).$$
(42)

This means that we neglect here non-Gaussian corrections to the distributions $f_i^{(0)}$ and hence, one expects to get simple but accurate expressions for the transport coefficients. With this approximation, $\zeta_i^{(0)}$ is

$$\begin{aligned} \zeta_{i}^{(0)} &= \frac{4\pi^{(d-1)/2}}{d\Gamma\left(\frac{d}{2}\right)} v_{0} \sum_{j=1}^{s} n_{j} \chi_{ij}^{(0)} \mu_{ji} \sigma_{ij}^{d-1} (1+\alpha_{ij}) \\ &\times \left(\frac{\beta_{i}+\beta_{j}}{\beta_{i}\beta_{j}}\right)^{1/2} \left[1-\frac{\mu_{ji}}{2} (1+\alpha_{ij})\frac{\beta_{i}+\beta_{j}}{\beta_{j}}\right], \quad (43) \end{aligned}$$

where $v_0(T) = \sqrt{2T/\overline{m}}$ is a thermal speed of the mixture, $\overline{m} = \sum_i m_i/s$, and $\beta_i = m_i T/\overline{m}T_i^{(0)}$. Furthermore, according to Eq. (29) the contribution η'_b to the bulk viscosity can also be computed by using the Maxwellian approximation (42) with the result

$$\eta_{\rm b}' = \frac{\pi^{(d-1)/2}}{d^2 \Gamma\left(\frac{d}{2}\right)} v_0 \sum_{i=1}^2 \sum_{j=1}^2 m_{ij} (1+\alpha_{ij}) \chi_{ij}^{(0)} n_i n_j \sigma_{ij}^{d+1} \\ \times \left(\frac{\beta_i + \beta_j}{\beta_i \beta_j}\right)^{1/2}.$$
(44)

To solve the integral equation (35), one takes the leading Sonine approximation to $\mathcal{D}_i(\mathbf{V})$

$$\mathcal{D}_{i}(\mathbf{V}) \to f_{i\mathrm{M}}(\mathbf{V})W_{i}(\mathbf{V})\frac{\overline{\omega}_{i}}{T_{i}^{(0)}},$$
 (45)

where

$$W_i(\mathbf{V}) = \frac{m_i V^2}{2T_i^{(0)}} - \frac{d}{2}.$$
 (46)

The relation between $\zeta^{(1,1)}$ and $\overline{\omega}_i$ can be easily obtained by substitution of Eq. (45) into Eq. (33). The result is

$$\zeta^{(1,1)} = \sum_{i=1}^{s} \, \xi_i \varpi_i, \tag{47}$$

where

$$\xi_{i} = \frac{3\pi^{(d-1)/2}}{2d\Gamma\left(\frac{d}{2}\right)} \frac{v_{0}^{3}}{nTT_{i}^{(0)}} \sum_{j=1}^{s} n_{i}n_{j}\sigma_{ij}^{d-1}\chi_{ij}^{(0)}m_{ij}\left(1-\alpha_{ij}^{2}\right) \\ \times (\beta_{i}+\beta_{j})^{1/2}\beta_{i}^{-3/2}\beta_{j}^{-1/2}.$$
(48)

The coefficients $\overline{\omega}_i$ can be finally obtained by substituting Eq. (45) into Eq. (35), multiplying it with $m_i V^2$, and integrating over the velocity. After some algebra, the corresponding set of coupled linear algebraic equations for the coefficients $\overline{\omega}_i$ are given by

$$\sum_{j=1}^{3} \left(\omega_{ij} + \frac{1}{2} \zeta^{(0)} \delta_{ij} + T_i^{(0)} \xi_j \right) \varpi_j = B_i, \qquad (49)$$

where

$$B_i = \frac{2}{d} T_i^{(0)} (1 - p^*) - T_i^{(0)} \zeta^{(1,0)} - T\phi \frac{\partial \gamma_i}{\partial \phi} - \frac{A_i}{d^2 n_i}, \quad (50)$$

and

$$\phi = \frac{\pi^{d/2}}{2^{d-1}d\Gamma\left(\frac{d}{2}\right)} \sum_{i=1}^{s} n_i \sigma_i^d \tag{51}$$

PHYSICAL REVIEW E 100, 032904 (2019)

is the solid volume fraction. Upon obtaining Eq. (50) we have taken into account that the dependence of the temperature ratios γ_i on the densities n_i is through their dependence on the mole fractions x_i and the volume fraction ϕ . Furthermore, the collision frequencies ω_{ij} are defined as

$$\omega_{ii} = \frac{1}{dn_i T_i^{(0)}} \left(\sum_{j=1}^s \int d\mathbf{v} m_i V^2 J_{ij}^{(0)} [f_{i,M} W_i, f_j^{(0)}] + \int d\mathbf{v} m_i V^2 J_{ii}^{(0)} [f_i^{(0)}, f_{i,M} W_i] \right), \quad (52)$$

$$\omega_{ij} = \frac{1}{dn_i T_j^{(0)}} \int d\mathbf{v} m_i V^2 J_{ij}^{(0)} [f_i^{(0)}, f_{j,M} W_j], \quad (i \neq j). \quad (53)$$

In the Maxwellian approximation (42), ω_{ii} and ω_{ij} are

a

$$\omega_{ii} = -\frac{\pi^{(d-1)/2}}{2dT_i^{(0)}\Gamma\left(\frac{d}{2}\right)} v_0^3 \left\{ \frac{3}{\sqrt{2}} n_i \sigma_i^{d-1} m_i \chi_{ii}^{(0)} \beta_i^{-3/2} \left(1 - \alpha_{ii}^2\right) \right. \\ \left. - \sum_{j \neq i}^s n_j m_{ij} \sigma_{ij}^{d-1} \chi_{ij}^{(0)} (1 + \alpha_{ij}) (\beta_i + \beta_j)^{-1/2} \beta_i^{-3/2} \right. \\ \left. \times \beta_j^{-1/2} \left[3\mu_{ji} (1 + \alpha_{ij}) (\beta_i + \beta_j) - 2(2\beta_i + 3\beta_j) \right] \right\},$$
(54)

$$\omega_{ij} = \frac{\pi^{(d-1)/2}}{2dT_j^{(0)}\Gamma(\frac{d}{2})} v_0^3 n_j m_{ij} \sigma_{ij}^{d-1} \chi_{ij}^{(0)} (1 + \alpha_{ij}) \times (\beta_i + \beta_j)^{-1/2} \beta_i^{-1/2} \beta_j^{-3/2} [3\mu_{ji} (1 + \alpha_{ij}) \times (\beta_i + \beta_j) - 2\beta_j].$$
(55)

In Eqs. (54) and (55), it is understood that $i \neq j$. The set of algebraic equations (52) can be now easily solved. In particular, for a binary mixture (s = 2) the solution of Eq. (49) for ϖ_1 can be written as

$$\overline{\omega}_{1} = \frac{B_{1}}{\omega_{11} - \frac{x_{1}}{x_{2}}\omega_{12} + \frac{1}{2}\zeta^{(0)} + T_{1}^{(0)}\left(\xi_{1} - \frac{x_{1}}{x_{2}}\xi_{2}\right)},$$
 (56)

where the relation $\varpi_2 = -(x_1/x_2)\varpi_1$ has been accounted for. The expression for ϖ_2 can be easily obtained from Eq. (56) by making the changes $1 \leftrightarrow 2$. The solution (56) is indeed consistent with the requirement $x_1\varpi_1 + x_2\varpi_2 =$ 0. This is because $x_1\gamma_1 + x_2\gamma_2 = 1$, $B_2 = -(x_1/x_2)B_1$, and $\omega_{11} - (x_1/x_2)\omega_{12} + \xi_1/x_1 = \omega_{22} - (x_2/x_1)\omega_{21} + \xi_2/x_2$.

The expression (56) provides ϖ_1 in terms of the parameters of the mixture. Its explicit form is relatively long and is omitted here for the sake of brevity. A simple but interesting case corresponds to ordinary mixtures (elastic collisions) where $\zeta^{(0)} = 0, \xi_i = 0, \gamma_i = 1, \beta_1 = 2\mu_{12}, \beta_2 = 2\mu_{21}, \text{ and } \varpi_1$ is

$$\varpi_{1} = \frac{4\pi^{d/2}}{d^{2}\Gamma(\frac{d}{2})}T\left(\omega_{11} - \frac{x_{1}}{x_{2}}\omega_{12}\right)^{-1}\left[n_{2}\sigma_{12}^{d}\chi_{12}^{(0)}(x_{2}\mu_{21} - x_{1}\mu_{12}) + \frac{1}{2}x_{2}\left(n_{1}\sigma_{1}^{d}\chi_{11}^{(0)} - n_{2}\sigma_{2}^{d}\chi_{22}^{(0)}\right)\right].$$
 (57)

Equation (57) differs from the one obtained by Jenkins and Mancini [4] for nearly elastic hard spheres (d = 3). This discrepancy is essentially due to the fact that the distribution functions of each species in Ref. [4] are assumed to be Maxwellian distributions even in inhomogeneous situations. This was already noted by the authors of this paper since they conclude that their expression for ϖ_1 could be improved by determining the perturbations to the Maxwellians using the Chapman-Enskog procedure [33]. Expression (57) accounts for not only the different centers **r** and **r** $\pm \sigma_{ij}$ of the colliding pair in the Enskog collision operator (2) but also for the form of the first-order distribution $f^{(1)}$ given by Eq. (24).

On the other hand, for a three-dimensional system (d = 3), the expression (57) for ϖ_1 agrees with the one derived in Ref. [31] [see Eq. (22d) of [31]] for a hard-sphere binary mixture. This confirms the relevant known limiting cases for the granular mixture results derived here for the temperature ratios.

Once the first-order contributions to the partial temperatures are known, the first-order contribution ζ_U to the cooling rate can be explicitly obtained by employing Eqs. (32), (33), (47), and (48). In addition, the second contribution η''_b to the bulk viscosity η_b can be obtained from Eq. (30). Thus, $\eta_b = \eta'_b + \eta''_b$ is completely determined from Eqs. (30) and (44). For elastic collisions ($\alpha_{ij} = 1$), as expected, the corresponding expression for η_b is consistent with previous works on ordinary mixtures [30–32].

V. BINARY GRANULAR MIXTURES

To illustrate the dependence of the coefficients ϖ_i , ζ_U , and $\eta_{\rm b}$ on the parameter space of the system, a binary mixture $(s = 2 \text{ and so}, \ \overline{\omega}_2 = -x_1 \overline{\omega}_1 / x_2)$ of inelastic hard spheres (d = 3) is considered. The above coefficients depend on many parameters: $\{x_1, T, m_1/m_2, \sigma_1/\sigma_2, \phi, \alpha_{11}, \alpha_{22}, \alpha_{12}\}$. A similar complexity also exists in the elastic limit [32], so the relevant new feature is the dependence of $\overline{\omega}_1$, ζ_U , and η_b on the coefficients of restitution. Moreover, for the sake of simplicity, the case of a common coefficient of restitution ($\alpha_{11} = \alpha_{22} =$ $\alpha_{12} \equiv \alpha$) of an equimolar mixture $(x_1 = \frac{1}{2})$ with $\sigma_1 = \sigma_2$ and solid volume fraction $\phi = 0.2$ (moderately dense gas) is considered. This reduces the parameter space to three quantities: $\{T, m_1/m_2, \alpha\}$. The dependence on temperature can be scaled out by introducing the (dimensionless) quantities $\varpi_1^* = (n\sigma_{12}^2 v_0/T) \varpi_1$ and $\eta_b^* \equiv \eta_b(\alpha)/\eta_b(1)$, where $\eta_b(1)$ is the bulk viscosity for elastic collisions. The coefficient ζ_U is dimensionless.

To display the dependence of the coefficients ϖ_1^* , η_b^* , and ζ_U on α , we have still to provide the form for the pair distribution function $\chi_{ij}^{(0)}$. In the case of spheres (d = 3), a good approximation of $\chi_{ij}^{(0)}$ is [34–36]

$$\chi_{ij}^{(0)} = \frac{1}{1-\phi} + \frac{3}{2} \frac{\phi}{(1-\phi)^2} \frac{\sigma_i \sigma_j M_2}{\sigma_{ij} M_3} + \frac{1}{2} \frac{\phi^2}{(1-\phi)^3} \left(\frac{\sigma_i \sigma_j M_2}{\sigma_{ij} M_3}\right)^2,$$
(58)

where $M_{\ell} = \sum_{i} x_i \sigma_i^{\ell}$. In Fig. 1, the (reduced) coefficient σ_1^* is plotted as a function of the coefficient of restitution α for several values of the mass ratio. It is quite apparent first that the influence of the inelasticity on σ_1^* is significant, specially for high mass ratios. With respect to the dependence on the



FIG. 1. The (reduced) coefficient ϖ_1^* as a function of the common coefficient of restitution α for a binary mixture of hard spheres (d = 3) with $x_1 = \frac{1}{2}$, $\sigma_1 = \sigma_2$, $\phi = 0.2$, and three different values of the mass ratio m_1/m_2 : $m_1/m_2 = 0.5$ (a), $m_1/m_2 = 4$ (b), and $m_1/m_2 = 10$ (c).

mass ratio, we see that while ϖ_1^* increases with inelasticity when $m_1/m_2 < 1$, the opposite happens when $m_1/m_2 > 1$. Furthermore, Fig. 1 also highlights that the magnitude of the first contribution to the partial temperature is in general quite small in comparison with the values of the remaining transport coefficients of the mixture [28,29]. To assess the impact of ϖ_1^* on the bulk viscosity and the first-order contribution to the cooling rate, Figs. 2 and 3 show the α dependence of the (reduced) coefficients $\eta_b(\alpha)/\eta_b(1)$ and ζ_U , respectively, for two values of the mass ratio. We also plot the corresponding values of these coefficients when $\overline{\omega}_1^*$ is neglected. Although both predictions (with and without $\overline{\omega}_1^*$) agree qualitatively, we observe that the effect of ϖ_1^* on both transport coefficients cannot be neglected specially for high mass ratios and moderate inelasticity (for instance, $\alpha \simeq 0.6$). This means that previous results [27,28] derived for both



FIG. 2. The (reduced) bulk viscosity $\eta_{\rm b}(\alpha)/\eta_{\rm b}(1)$ as function of the common coefficient of restitution α for а а binary mixture of hard spheres (d = 3) with $x_1 = \frac{1}{2}$, $\sigma_1 = \sigma_2$, $\phi = 0.2$, and two different values of the mass m_1/m_2 : $m_1/m_2 = 0.5$ (a) and $m_1/m_2 = 10$ ratio (b). The dashed lines are the results for the (reduced) bulk viscosity when the contribution η_b'' to η_b is neglected.



FIG. 3. Magnitude of the (reduced) coefficient ζ_U as a function of the common coefficient of restitution α for a binary mixture of hard spheres (d = 3) with $x_1 = \frac{1}{2}$, $\sigma_1 = \sigma_2$, $\phi = 0.2$, and two different values of the mass ratio m_1/m_2 : $m_1/m_2 = 0.5$ (a) and $m_1/m_2 = 10$ (b). The dashed lines are the results for the coefficient ζ_U when the contribution $\zeta^{(1,1)}$ to ζ_U is neglected.

the bulk viscosity and the cooling rate of granular mixtures must be slightly changed when the masses of the constituents of the mixture become very disparate and/or the collisional dissipation becomes significant.

VI. CONCLUDING REMARKS

One of the most intriguing differences between ordinary and granular mixtures is the absence of energy equipartition in homogeneous states. This means that the zeroth-order contributions $T_i^{(0)}$ to the *partial* temperatures T_i (measuring the mean kinetic energy of each species) of granular mixtures are different for mechanically different components, reflecting a violation of the equipartition theorem valid for elastic collisions [9]. The origin of this violation is the inelasticity in collisions, and its impact on transport problems such as thermal diffusion segregation [37–39] has been shown to be quite significant, specially for strong dissipation and/or disparate mass ratios.

In addition, as was already noted in some of the pioneering papers of the Enskog theory for multicomponent ordinary mixtures [30–32], a breakdown of energy equipartition is also present in the Navier-Stokes domain (first-order in spatial gradients) for moderately dense mixtures. The origin of this violation is associated with the spatial gradients, and more specifically with the divergence of flow velocity since the first-order contributions $T_i^{(1)}$ to the partial temperatures are proportional to $\nabla \cdot \mathbf{U}$. This additional source of energy nonequipartition is independent of the one appearing in the homogeneous cooling state for granular mixtures.

On the other hand, the coefficients $T_i^{(1)}$ are usually neglected in many of the works devoted to granular mixtures [5,27,28] because only the first terms in the Sonine polynomial expansion are retained. Since $T_i^{(1)} \propto \nabla \cdot \mathbf{U}$, an interesting question is to assess the impact of the first-order coefficients $T_i^{(1)}$ on both the bulk viscosity η_b and the firstorder contribution ζ_U to the cooling rate.

The goal of this paper has been to determine the coefficients $T_i^{(1)}$ from the Chapman-Enskog solution to the (inelastic) version of the Enskog kinetic equation [3]. As in previous works [27,28], this task has been achieved in two different steps. First, we have obtained in an exact way the set of linear integral equations that the first-order contributions $T_i^{(1)}$ satisfy. This has allowed us to prove the solubility condition for solving this set of integral equations. As a second step, an approximate solution to the above set of equations is required for practical purposes in order to explicitly express the coefficients $T_i^{(1)}$ in terms of the parameter space of the problem (masses, diameters, composition, density, and coefficients of restitution). This task has been achieved by considering the leading terms in the Sonine polynomial expansion. Thus, the results derived here for $T_i^{(1)}$ extend to inelastic collisions the calculations performed many years ago [30-32] for ordinary hard-sphere mixtures. Moreover, the expressions obtained here for η_b [given by Eqs. (28)–(30)] and ζ_U [given by Eqs. (32), (47), and (48)] correct the previous results derived in Refs. [27,28] where the contributions η_b'' and $\zeta^{(1,1)}$ to η_b and ζ_U , respectively, were implicitly neglected.

For the sake of illustration and to assess the impact of $T_i^{(1)}$ on η_b and ζ_U , a binary mixture with a common coefficient of restitution ($\alpha_{ij} \equiv \alpha$) has been considered to analyze the dependence of the above transport coefficients on inelasticity. First, as Fig. 1 shows, we observe that the effect of inelasticity on the first-order contributions to the partial temperatures is in general quite important, specially for large mass ratios. With respect to the influence of $T_1^{(1)}$ on η_b and ζ_U , Figs. 2 and 3 highlight that the impact of the first-order partial temperature on both the bulk viscosity and the cooling rate can be relatively important for moderate inelasticity and/or disparate mass ratios.

An interesting problem is to extend the present results to the case of polydisperse granular mixtures driven by a stochastic bath with friction [40–42]. This kind of thermostat models the effect of the surrounding interstitial viscous gas on the dynamics of grains (granular suspensions). An extensive study on the transport coefficients for driven granular mixtures at low density has been carried out in Refs. [43–45]. In contrast with the findings reported here for *freely* cooling granular dilute gases (where $T_i^{(1)} = 0$ when $\phi = 0$), the results derived for driven systems [45] show that the first-order contributions $T_i^{(1)}$ to the partial temperatures are different from zero even when $\phi = 0$. The extension of the results obtained in Refs. [43–45] to finite density is an interesting project. Work along this line will be initiated in the near future.

In summary, we have revisited previous works on polydisperse granular mixtures [27,28] where the first-order contributions $T_i^{(1)}$ to the partial temperatures were neglected. The present work fixes the above limitation by including not only the calculation of $T_i^{(1)}$ but also their influence on the bulk viscosity η_b and on the first-order contribution ζ_U to the cooling rate. Our results show first that the first-order coefficients $T_i^{(1)}$ exhibit in general a complex dependence on the coefficients of restitution of the mixture. In addition, they also show that the impact of $T_i^{(1)}$ on both η_b and ζ_U cannot be neglected for disparate masses and/or strong dissipation. In this context, the results derived before for polydisperse dense granular mixtures [27,28] must be slightly modified by including the contributions coming from the partial temperatures $T_i^{(1)}$ to the transport properties and the cooling rate.

ACKNOWLEDGMENTS

We are grateful to Dr. Mariano López de Haro for a critical reading of the manuscript and for calling our attention to

- N. Brilliantov and T. Pöschel, *Kinetic Theory of Granular Gases* (Oxford University, Oxford, 2004).
- [2] K. K. Rao and P. R. Nott, *An Introduction to Granular Flow* (Cambridge University, Cambridge, England, 2008).
- [3] V. Garzó, Granular Gaseous Flows (Springer Nature Switzerland, Basel, 2019).
- [4] J. T. Jenkins and F. Mancini, J. Appl. Mech. 54, 27 (1987).
- [5] J. T. Jenkins and F. Mancini, Phys. Fluids A 1, 2050 (1989).
- [6] P. Zamankhan, Phys. Rev. E 52, 4877 (1995).
- [7] B. Arnarson and J. T. Willits, Phys. Fluids 10, 1324 (1998).
- [8] J. T. Willits and B. Arnarson, Phys. Fluids 11, 3116 (1999).
- [9] V. Garzó and J. W. Dufty, Phys. Rev. E 60, 5706 (1999).
- [10] P. A. Martin and J. Piasecki, Europhys. Lett. 46, 613 (1999).
- [11] J. M. Montanero and V. Garzó, Granular Matter 4, 17 (2002).
- [12] A. Barrat and E. Trizac, Granular Matter 4, 57 (2002).
- [13] S. R. Dahl, C. M. Hrenya, V. Garzó, and J. W. Dufty, Phys. Rev. E 66, 041301 (2002).
- [14] R. Pagnani, U. M. Bettolo Marconi, and A. Puglisi, Phys. Rev. E 66, 051304 (2002).
- [15] P. E. Krouskop and J. Talbot, Phys. Rev. E 68, 021304 (2003).
- [16] H. Q. Wang, G. J. Jin, and Y. Q. Ma, Phys. Rev. E 68, 031301 (2003).
- [17] J. J. Brey, M. J. Ruiz-Montero, and F. Moreno, Phys. Rev. Lett. 95, 098001 (2005).
- [18] M. Schröter, S. Ulrich, J. Kreft, J. B. Swift, and H. L. Swinney, Phys. Rev. E 74, 011307 (2006).
- [19] R. D. Wildman and D. J. Parker, Phys. Rev. Lett. 88, 064301 (2002).
- [20] K. Feitosa and N. Menon, Phys. Rev. Lett. 88, 198301 (2002).
- [21] V. Garzó and J. W. Dufty, Phys. Fluids 14, 1476 (2002).
- [22] D. Serero, I. Goldhirsch, S. H. Noskowicz, and M. L. Tan, J. Fluid Mech. 554, 237 (2006).
- [23] V. Garzó, J. M. Montanero, and J. W. Dufty, Phys. Fluids 18, 083305 (2006).

the papers [30,31]. The present work has been supported by the Spanish Government through Grant No. FIS2016-76359-P and by the Junta de Extremadura (Spain) Grants No. IB16013 (V.G.) and No. GR18079, partially financed by "Fondo Europeo de Desarrollo Regional" funds. The research of R.G.G. has been supported by the predoctoral fellowship BES-2017-079725 from the Spanish Government.

- [24] V. Garzó and J. M. Montanero, J. Stat. Phys. 129, 27 (2007).
- [25] D. Serero, S. H. Noskowicz, M. L. Tan, and I. Goldhirsch, Eur. Phys. J. ST **179**, 221 (2009).
- [26] V. Garzó, J. A. Murray, and F. Vega Reyes, Phys. Fluids 25, 043302 (2013).
- [27] V. Garzó, J. W. Dufty, and C. M. Hrenya, Phys. Rev. E 76, 031303 (2007).
- [28] V. Garzó, C. M. Hrenya, and J. W. Dufty, Phys. Rev. E 76, 031304 (2007).
- [29] J. A. Murray, V. Garzó, and C. M. Hrenya, Powder Technol. 220, 24 (2012).
- [30] J. Karkheck and G. Stell, J. Chem. Phys. 71, 3620 (1979).
- [31] J. Karkheck and G. Stell, J. Chem. Phys. 71, 3636 (1979).
- [32] M. López de Haro, E. G. D. Cohen, and J. Kincaid, J. Chem. Phys. 78, 2746 (1983).
- [33] S. Chapman and T. G. Cowling, *The Mathematical Theory of Nonuniform Gases* (Cambridge University, Cambridge, England, 1970).
- [34] T. Boublik, J. Chem. Phys. 53, 471 (1970).
- [35] E. W. Grundke and D. Henderson, Mol. Phys. 24, 269 (1972).
- [36] L. L. Lee and D. Levesque, Mol. Phys. 26, 1351 (1973).
- [37] V. Garzó, Phys. Rev. E 78, 020301(R) (2008).
- [38] V. Garzó, Eur. Phys. J. E 29, 261 (2009).
- [39] V. Garzó, New J. Phys. 13, 055020 (2011).
- [40] A. Puglisi, V. Loreto, U. M. B. Marconi, A. Petri, and A. Vulpiani, Phys. Rev. Lett. 81, 3848 (1998).
- [41] A. Sarracino, D. Villamaina, G. Gradenigo, and A. Puglisi, Europhys. Lett. 92, 34001 (2010).
- [42] A. Sarracino, D. Villamaina, G. Costantini, and A. Puglisi, J. Stat. Mech. (2010) P04013.
- [43] N. Khalil and V. Garzó, Phys. Rev. E 88, 052201 (2013).
- [44] N. Khalil and V. Garzó, Phys. Rev. E 97, 022902 (2018).
- [45] N. Khalil and V. Garzó, Phys. Rev. E 99, 059901(E) (2019).